 DRAFT REV. 4 dtd 12 Sep 2011

Business Plan for Electric Power Production and Manufacturing for the Turtle Mountain Chippewa Band, Belcourt, North Dakota

20 MWe (net electric output) Coal and Biomass Fired Steam Plant, 90%+ Emissions Capture Capability with Chemical Byproducts Co-Production, Using Pipeline Natural Gas for Co-Product Manufacture Only

Representative facility: Twin 24 MWe Delano Biomass Power Plant, California

For assistance in arranging of project financing, cost analyst services and project liaison,

please contact: Walter James O'Brien, power plant cost consultant

E-mail: W_James_Obrien@myway.com

Tel: (607) 343-7452

← ESTIMATES AND GENERAL SPECIFICATIONS

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I. Executive Summary

There are several million tonnes of deciduous and evergreen tree trimming and timber waste harvested and reposited at most municipal landfills in North Dakota which are suitable for power plant fuel utilization. This proposed power plant, intended to be ultimately a complex of (5) 20 MWe power modules, shall co-fire coal and biomass in the appropriate ratio to achieve the following goals to support Turtle Mountain Chippewa economic growth and independence.

1. Provide electrical power to the grid using the business model of the public-private partnership;

2. Provide steam to industrial clients at neighboring independent sites;

3. Co-produce using carbon capture technology and conventional chemical refinery practice such products as plastics for injection molding manufacturing feedstock, synthetic Diesel fuel and synthetic natural gas for transportation fleet service, methanol, ethanol, fly ash for road construction, gypsum for wallboard manufacture, ammonium sulfate fertilizer, and a range of other products exclusively for sale to industrial enterprises or for government use in reducing its fuel use bill;

4. Provide all of the above while maintaining a 90+ % rate of GHG emissions sequestration of flue gas emissions into the manufactured commodities as listed in Item 3.

5. With growth, this facility will also serve as a processing and marketing facility for CO2 delivered from other sites which have captured CO2.

Supplementary environmental projects which would support community development should include the following:

1. Establishment of a well-paid trades apprenticeship program in conjunction with the unions and utilities for the training of boiler and steam turbine operator and repair/maintenance technicians, solid fuel boiler specialist technicians, and hydrocarbon refinery repair and operations technicians.

II. General Enterprise Description

Mission Statement: This proposed public-private partnership provides electric power, chemical byproduct, consulting services, and technical apprenticeship training in an environmentally-sound manner which likewise meets and exceeds client expectations for price, delivery, specifications compliance and quality.

III. PRODUCTS AND SERVICES

Electric power shall be supplied to the grid in accordance with NERC, FERC, APPA or NRECA, IEEE and other technical and regulatory specifications, terms and conditions in modules of 20 MWe to match the appropriate line voltage, phase, frequency and signal quality specified.

The principal chemical products manufactured from this flue gas emissions-based co-production manufacturing regime shall be the following:

A. Ammonium sulfate using the Marsulex method and technology

B. Gypsum from fly ash using the Marsulex method and technology.

C. Urea, ammonia, synthetic Diesel fuel, ethanol, methanol, and synthetic natural gas in either liquid or prilled form using licenced technology from either Linde Gases, Selas Liquid Processing Division, Uhde gmbH of Germany or Stamicarbon.

D. Product lines fine-tuned to the needs of the plastics, coatings and other liquid hydrocarbon needs of pertinent manufacturers.

Please see attached standards compliance documents describing the finished business to business industrial feedstock products to be supplied by the proposed flue gas emission-based manufacturing facility and power plant.

Respecting marketing advantages inherent in this business model, the proposed plant has electrical sales to offset the cost of chemical manufacture and vice versa. This is why the plant is referred to as a “co-production” plant. This gives the facility the ability to track cost-effectively fluctuations in commodity market conditions and prices. As well, no activity shall be engaged in at this facility which does not reflect the highest standards in insurance standard-regulated compliance for both environmental and safety standards, making of this a genuinely sustainable enterprise. As a consulting and training tool, the proposed facility provides hands-on operational equipment and functional industrial examples for both the consultant and the apprentice to reference and quantify, both for the benefit of the client and for the benefit of the apprentice.

It would be the height of dishonesty and naivete to state that the need for supplementary natural gas usage is not going to be a significant economic factor. That being said, the “killer” cost in chemical plant operations has always been the cost of making steam, as the heat generation amounts to a dead write-off in one’s pro forma manufacturing spreadsheet unless one is co-generating electric power and selling steam to another facility and unless the fuel used for the steam generation phase is very cheap, which in both instances we are doing here in combining functions of electric and steam generation for off-site end-users while making chemical byproducts. All of the natural gas will be used solely for hydrocarbon feedstock for catalytic steam reforming, not steam generation, and thus those hydrocarbon molecules are fully monetized.

While the majority of the alternative and renewables industry are scratching their heads as to where to sell electricity and biodiesel-based byproduct at an indexed-commodity derivatives trader-friendly basis, this plant will address the practical realities of the needs and requests of the market place in both electrical power and in commodities supply. The three key elements of the facility's marketing strategy are as follows:

1. to provide electric power on a cost plus fixed percentage basis into the grid, allowing the distribution and transmission provider to set the rates to the retail and wholesale market as they choose;

2. to provide chemical co-production commodities at a cost plus fixed percentage basis to all indexed-supply side distributors on an equal footing for marketing by them in accordance with their derivative-trader-based yield expectations; and

3. to provide both of the above with a committed view to meld such activities into the individual corporate growth plans of local enterprise with the view to maximize living-wage sustainable employment while helping participating firms to maximize their shareholders' stock yield expectations.

This strategy gives this project the ultimate in market flexibility while preserving a competitive cost edge over all other suppliers, and likewise while successfully meeting facility cash flow needs and conservative shareholder expectations. In other words, marketing is based not on what we tell the customer it will cost for our goods, but rather on what our customer wants and needs to maintain their edge in the wholesale distribution arena of competition. By maintaining our course in the cost plus fixed-percentage mode and refusing the derivatives traders' back-door commission, the co-production plant will be insulated from the vagaries of commodity speculation regardless of the condition of the American industrial economy.

The other principal market advantage is a product of accepting that underground carbon sequestration is not economically viable, and the only alternative is one that will yield a conventional profit. The monetization of carbon dioxide and other flue gas emission chemicals, fortunately, enjoys a chemical industrial tradition of conventionally profitable efficacy which dates back to well before the First World War, both in North America and in Europe.

There is nothing unique nor radically innovative in the design of the basic plant module array. All aspects of this operation's array can be viewed in operation at the Bismarck, ND Dakota Gasification plant, of which this is little more than a

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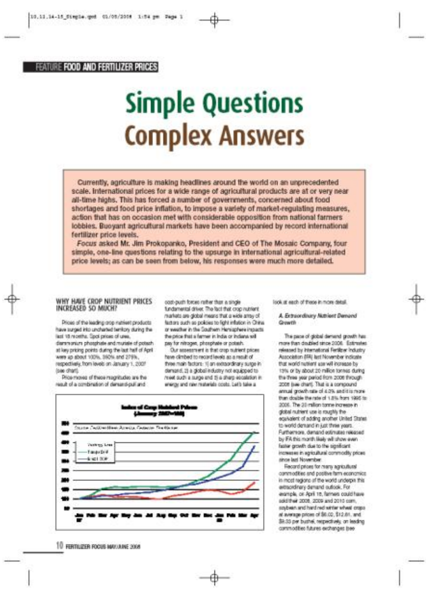
scaled-down version except that it co-fires with wood and/or wood waste products to satisfy raw emissions reduction requirements. Each and every component and subsystem is an insurance and safety inspector's source of confidence in the viability and sustainability of the enterprise. There is no component nor subsystem of the proposed plants which has not at least a fifty-year history of successful and profitable operation in industrial practice, save in the area of upgraded digital control components which likewise are a product of rigid and inflexible insurance inspection bureau enforced safety and performance standards and specifications controls.

IV. Marketing Plan

The aim of the enterprise's commodity and services marketing team is to establish long-term relationships contractually (five years or more) with a range of industrial clients who in turn supply OEM (original equipment manufacturer) parts and subcomponents, trained workers, design services & consulting to other clients. This provides for the Turtle Mountain Chippewa band's energy planners the basis for stability, predictability and long-term planning that makes for orderly growth.

Ammonium sulfate fertilizer and urea fertilizer are to be our prime focii for the fertilizer market. Our aim is first to service the local market through existing fertilizer brokers, not to undermine nor compete with them, but to provide to the local brokers a substantially less expensive product to increase their competitiveness which is locally made using local workers to build a stronger local economy and tax base. The following documents provide an overview of the market for fertilizer globally as a whole.



FEATURE FOOD AND FERTILIZER PRICES

Simple Questions
Complex Answers

Currently, agriculture is making headlines around the world on an unprecedented scale. International prices for a wide range of agricultural products are at or very near all-time highs. This has forced a number of governments, concerned about food shortages and food price inflation, to impose a variety of market-regulating measures, action that has on occasion met with considerable opposition from national farmers lobbies. Buoyant agricultural markets have been accompanied by record international fertilizer price levels.

Focus asked Mr. Jim Prokopanko, President and CEO of The Mosaic Company, four simple, one-line questions relating to the upsurge in international agricultural-related price levels; as can be seen from below, his responses were much more detailed.

WHY HAVE CROP NUTRIENT PRICES INCREASED SO MUCH?

Prices of the leading crop nutrient products have surged into uncharted territory during the last 18 months. Spot prices of urea, diammonium phosphate and muriate of potash at key pricing points during the last half of April were up about 100%, 350% and 275%, respectively, from levels on January 1, 2007 (see chart).

Price moves of these magnitudes are the result of a combination of demand-pull and cost-push forces rather than a single fundamental driver. The fact that crop nutrient markets are global means that a wide array of factors such as policies to fight inflation in China or weather in the Southern Hemisphere impacts the price that a farmer in India or Indiana will pay for nitrogen, phosphate or potash.

Our assessment is that crop nutrient prices have climbed to record levels as a result of three main factors: 1) an extraordinary surge in demand, 2) a global industry not equipped to meet such a surge and 3) a sharp escalation in energy and raw materials costs. Let's take a look at each of these in more detail.

A. Extraordinary Nutrient Demand Growth

The pace of global demand growth has more than doubled since 2006. Estimates released by International Fertilizer Industry Association (IFA) last November indicate that world nutrient use will increase by 13% or by about 20 million tonnes during the three year period from 2006 through 2008 (see chart). That is a compound annual growth rate of 4.0% and it is more than double the rate of 1.8% from 1996 to 2006. The 20 million tonne increase in global nutrient use is roughly the equivalent of adding another United States to world demand in just three years. Furthermore, demand estimates released by IFA this month likely will show even faster growth due to the significant increases in agricultural commodity prices since last November.

Record prices for many agricultural commodities and positive farm economics in most regions of the world underpin this extraordinary demand outlook. For example, on April 18, farmers could have sold their 2008, 2009 and 2010 corn, soybean and hard red winter wheat crops at average prices of $6.02, $12.81, and $9.33 per bushel, respectively, on leading commodities futures exchanges (see

10 FERTILIZER FOCUS MAY/JUNE 2008

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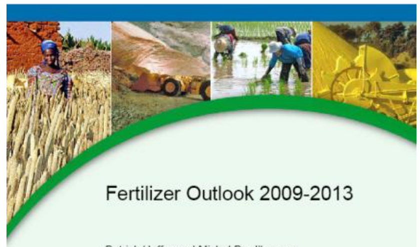
International Fertilizer Industry Association

A/09/87
June 2009

77th IFA Annual Conference
Shanghai (China P.R.), 25-27 May 2009



Fertilizer Outlook 2009-2013

Patrick Heffer and Michel Prud'homme
International Fertilizer Industry Association (IFA)

International Fertilizer Industry Association (IFA) – 28, rue Marbeuf – 75008 Paris – France
Tel. +33 1 53 93 05 00 – Fax +33 1 53 93 05 45/47 – ifa@fertilizer.org – www.fertilizer.org

THE MARKET
FERTILIZER NEWS AND ANALYSIS FROM ICIS
NITROGEN | PHOSPHATES | AMMONIA | SULPHUR | POTASH | NEWS | PRICES
VOL 12 No 31 3 SEPTEMBER 2009

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ICIS pricing fertilizers
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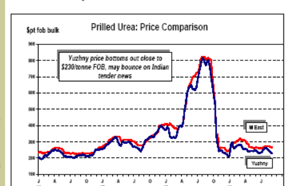
rebecca.clarke@icis.com
carl.roache@icis.com
mike.nash@icis.com
Web: www.icispricing.com

Nitrogen

OVERVIEW

The latest dip in the urea market has bottomed out this week at $228-230/tonne FOB Yuzhny. The surprise announcement of a new Indian tender on 3 September prompted a move to cover short sales. Traders stepped in and bought tonnage in Yuzhny in mid week at that level.

Ukrainian producers have raised their asking prices in response and are seeking $240/tonne FOB or higher once again, which may kill off some demand. Traders face a tricky decision over the coming week, calculating at what price they should offer in the Indian tender on 10 September.



The Indian buyers have timed their entry to the market to coincide with a low point in prices and will probably target levels below $270/tonne CFR. Based on freight of $33/tonne for panamax cargoes from the Black Sea, this implies a purchase price in Yuzhny of around $230/tonne allowing for a small margin and other costs.

Chinese urea is unlikely to feature in the Indian tender as the shipment period coincides with the return to a 110% export tax rate. Middle East producers have urea to sell for late September and October and will probably seek to maintain prices above $260/tonne FOB, implying the mid/high-$270s/tonne CFR for handysize cargoes. In addition, Iranian, Omani, Egyptian and Indonesian urea are likely to be offered.

Indian buying may prompt buyers in other countries to firm up their inquiries and purchase quickly for September loading.

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IV. MARKETING PLAN (continued)

Gypsum for wallboard manufacture and fly ash for road construction

Gypsum production, like the fertilizer products, shall be dependent on the Marsulex™ process. Local manufacturers of wallboard shall have first priority, and spot market prices shall be consulted to ensure the gypsum is priced competitively. Fly ash marketing shall be local in character to road building contractors first, based upon the chemical and American Concrete Institute specification with which the fly ash must comply; this product may need secondary processing, and the Israel design & implementation team will seek out the appropriate firm to address this possible requirement. Please see below for a simplified technical description as to how the Marsulex™ process works. Marsulex™ is the preferred process for ammonium sulfate and gypsum extraction, as they have over 120 operational and successful installations on coal plants globally, and are headquartered in Lebanon, PA.

MARSULEX
ENVIRONMENTAL TECHNOLOGIES

Ammonium Sulfate WFGD Technology
OVERVIEW FOR GENERAL INDUSTRY INFORMATION
July 2007

Background

Marsulex Environmental Technologies (MET) has developed an effective ammonia scrubbing technology that removes sulfur dioxide (SO_2) from boiler flue gases and produces high-value ammonium sulfate (AS) fertilizer. The AS scrubbing system uses proven wet flue gas desulfurization (WFGD) equipment and therefore can achieve the same high reliability of the more traditional limestone-based WFGD. The produced high-value AS fertilizer enhances the project economics.

The first field pilot of this technology was successfully executed at the Dakota Gasification (DGC) facility in the early 1990's and led to a subsequent full-scale commercial installation at that site. This AS WFGD system has been scrubbing flue gas and producing fertilizer in accordance with design for well over 10 years now. In late 2006, the second commercial application of the AS WFGD went into operation at the Syncrude Upgrading Expansion – Phase 1 (UE-1) Project in Alberta, Canada.

The MET AS WFGD process is similar to the more familiar limestone/gypsum WFGD process as illustrated in Figure 1. In fact, many components are common between these two processes, such as the absorber vessel, recycle pumps, spray nozzles, etc. The equipment components which differ are reagent handling and dewatering. Limestone-based WFGD usually requires a fairly complex reagent slurry preparation system consisting of a limestone storage silo, weigh feeder, wet ball mill with all required accessory equipment, cyclone classifier, ball mill product sump with agitator, ball mill product pumps, limestone slurry tank and limestone slurry feed pumps. In comparison, the simpler AS WFGD ammonia feed system consists of an ammonia storage tank, ammonia feed pumps and a vaporizer in the event of anhydrous ammonia supply. The AS WFGD process employs centrifuges for dewatering, in lieu of belt or rotary drum filters, based on their ability to produce a low moisture cake and smaller plot area requirement.

Economics

The favorable economics of the MET AS-FGD technology resides in the ability to process low cost, high sulfur coals while generating a high-value fertilizer product. The economic model of the AS-FGD favors higher sulfur in the fuel via the increased AS production rate and potential for higher net

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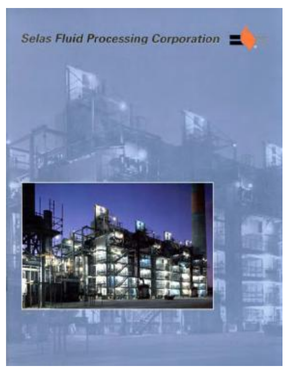
Synthetic Diesel fuel and synthetic natural gas for transportation fleet service, methanol, ammonia, urea and ethanol

The process to be used in manufacturing shall be catalytic steam reforming as provided under license from either KBR, Uhde gmbH or Linde Gases, Inc., applying the captured CO2 plus steam to the reformer and passage of the mix through the reformer's catalytic cracking array. Linde Gases, Inc., are the preferred vendor, as their experience traces back fifty years, and they are headquartered close by in Blue Bell, PA. Please see the following technical literature for an overview of the vendor and the process. Again, unless the time, money and expense of investing in a gasification array is to be undertaken, the plan is to use natural gas from an on-site pipeline to serve as the provider of feedstock for the catalytic steam reforming process, NOT for the steam generating aspect. Steam is expensive to make with natural gas, but the biomass-coal combination solves that problem while making it possible to monetize at its maximum yield ALL the natural gas provided to the system.




Selas Fluid Reformers

Global Experience in Steam Reforming

The Technology

Did you know...

How carbon capture is to be achieved using UOP CO2 membrane filters which is to be located downstream of the Marsulex unit as part of the final flue gas ductwork and is non-technically described below as well. . The toxic byproducts of wood combustion, unaddressed in most biomass combustion arrays (toluene, benzene, highly mutagenic organics, heavy metals, etc.) as described in the

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attached .XLS Environmental Protection Agency document (please see right hand table tabbed ALLOTHERPLLNTS), will also be removed to a concentration of less than both commercial sanitary food grade standards and the emission standards of all other known biomass plants in the country for chemical purity, including soft drink manufacturers. No untried nor uninsurable prototypes will be part of this plant.

Verantis

EPA wood toxins

V. Operational Plan

Financing phase

1. Presentation of prospectus to targeted equity participants to time of equity participation acceptance: 90 days

2. Parallel activities (obtaining letters of intent to buy co-production commodities from fertilizer and chemical firms, crafting of power purchase agreement with interested parties, etc.): 90 days

3. Obtaining of funding for feasibility study from targeted equity participants: 60 days

4. Obtaining of letters of intent on project funding from equity participant(s): 60 days

5. Purchasing of underwriting insurance for the overall project funding from appropriate specialist underwriting firm: 30 days

6. "Calling" of the letters of intent from equity participants: 30 days

7. Due diligence respecting applications for environmental permits: 2-4 years

8. Other due diligence qualifying facility filings: 1 year

9. Finalizing of Power purchase agreements 2 years

10. Crafting and issuance of RFP's to contractors for construction: 1 year

11. Groundbreaking upon award of construction contracts

Construction and commissioning phase

(Conducted under the guidance of the construction management team)

Delivery of the last of the major components: 1 year

Organizational planning, tactical detail development and deployment of the managerial team (concurrent with construction phase initiation): 1 year

Time to completion of construction from groundbreaking date: 2.5-3.0 years

Training of operations and maintenance crews: 6 months

Commissioning and shakedown of the facility (concurrent with above training activities): 6 months

Production phase

Commence delivery of electric power to grid

Commence marketing, manufacture and delivery of chemical byproducts

Commence research efforts on new applications for oxy-fuel burners

Commence consulting to the electric utility, steel, chemical and refining industries to aid them in installing and commissioning similar arrays.

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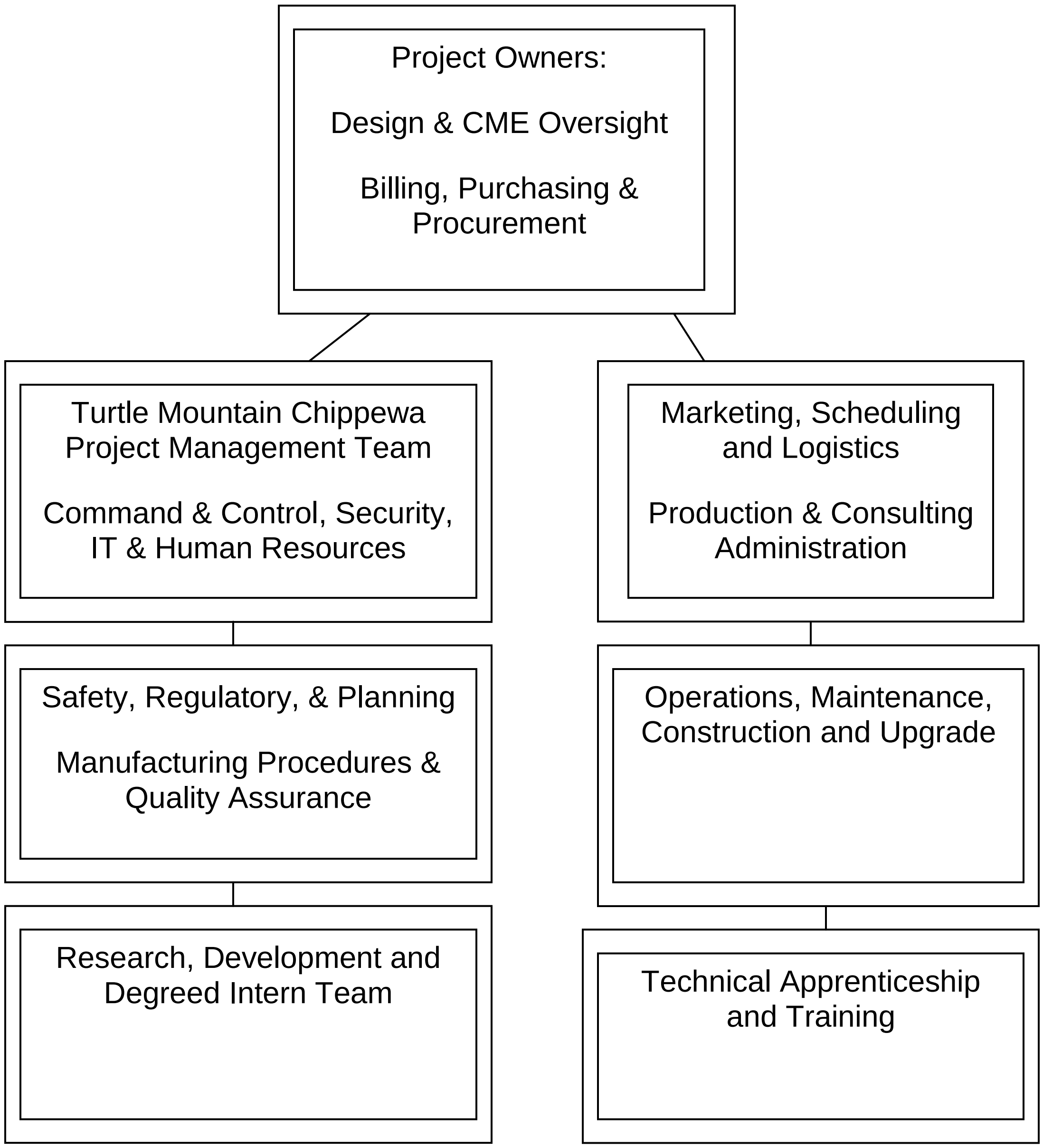
VI. Management and Organization (Proposed)



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VII. Appendices

Int. J. Environmental Technology and Management, Vol. 4, Nos. 1/2, 2004 89

Aqua ammonia process for simultaneous removal of CO_2, SO_2 and NO_x

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Abstract: Experimental research work in applying aqueous ammonia solution for the simultaneous reduction of acidic gaseous emission from fossil fuel-fired utility plants is currently being performed at the National Energy Technology Laboratory. The traditional monoethanolamine process for CO_2 removal suffers the disadvantages of low carbon dioxide loading capacity, equipment corrosion, amine degradation by SO_2 and O_2 in flue gas, and high energy penalty during absorbent regeneration. The aqueous ammonia process can simultaneously remove CO_2, SO_2, NO_x, plus HCl and HF that may exist in the flue gas. There could be oxidation of SO_2 and NO prior to contacting the aqueous ammonia absorbent. Test results pertaining to the ammonia/carbon dioxide reaction in a semi-continuous reactor system are presented. The parametric effects of sparger design, reaction temperature, and ammonia concentration on gas loadings and absorption rates are discussed. Regeneration test results, including solution-cycling between the regeneration and absorption steps to determine a realistic loading capacity for the ammonia solutions are also presented.

Keywords: absorption, aqueous ammonia, ammonium bicarbonate, ammonium nitrate, ammonium sulfate, carbon dioxide loading, desulfurisation, fertilizer, heat of reaction, monoethanolamine, oxidation, regeneration.

Reference to this paper should be made as follows: Resnik, K.P., Yeh, J.T. and Pennline, H.W. (2004) 'Aqua ammonia process for simultaneous removal of CO_2, SO_2 and NO_x', Int. J. Environmental Technology and Management, Vol. 4, Nos. 1/2, pp.89–104.

Biographical notes: K.P. Resnik is a Process Engineer with Parson Project Services, Inc., the site-support contractor for the in-house operations at the US Department of Energy's National Energy Technology Laboratory. He has worked with air pollution abatement systems over the past 15 years.

J.T. Yeh is a Project Leader with the DOE and has been involved in environmental projects in the past.

H.W. Pennline is a Team Leader in the carbon dioxide capture area responsible for various projects in the sequestration area.

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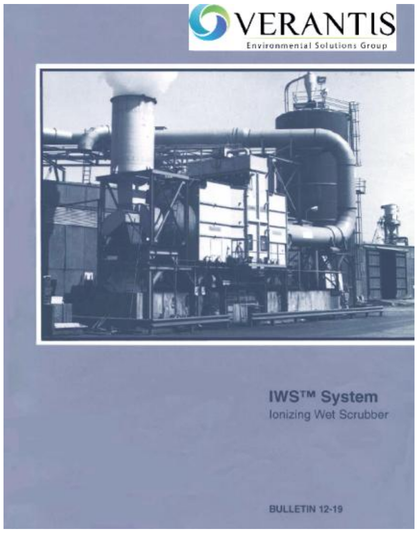
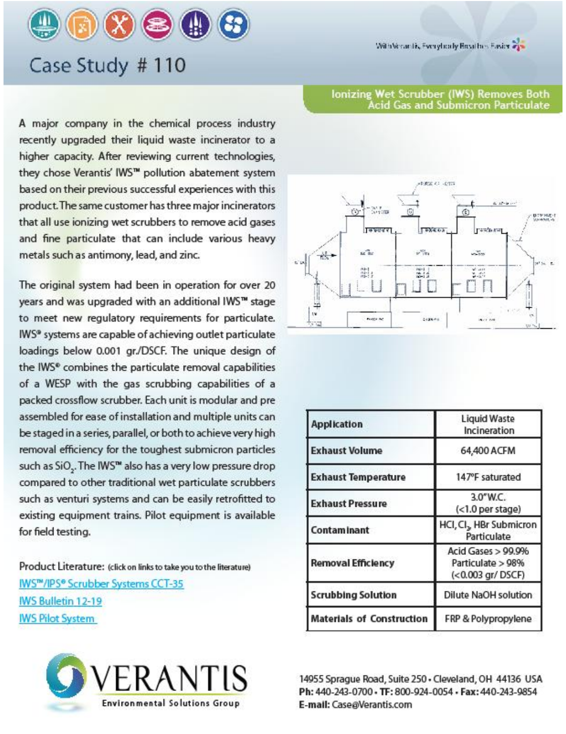
Ammonia Based CO2/S0x/N0x Removal





Case Study # 110

With Verantis, Everybody Breathes Easier

Ionizing Wet Scrubber (IWS) Removes Both Acid Gas and Submicron Particulate

A major company in the chemical process industry recently upgraded their liquid waste incinerator to a higher capacity. After reviewing current technologies, they chose Verantis' IWS™ pollution abatement system based on their previous successful experiences with this product. The same customer has three major incinerators that all use ionizing wet scrubbers to remove acid gases and fine particulate that can include various heavy metals such as antimony, lead, and zinc.

The original system had been in operation for over 20 years and was upgraded with an additional IWS™ stage to meet new regulatory requirements for particulate. IWS® systems are capable of achieving outlet particulate loadings below 0.001 gr./DSCF. The unique design of the IWS® combines the particulate removal capabilities of a WESP with the gas scrubbing capabilities of a packed crossflow scrubber. Each unit is modular and pre assembled for ease of installation and multiple units can be staged in a series, parallel, or both to achieve very high removal efficiency for the toughest submicron particles such as SiO_2. The IWS™ also has a very low pressure drop compared to other traditional wet particulate scrubbers such as venturi systems and can be easily retrofitted to existing equipment trains. Pilot equipment is available for field testing.

Product Literature: (click on links to take you to the literature)
IWS™/IPS® Scrubber Systems CCT-35
IWS Bulletin 12-19
IWS Pilot System

Application	Liquid Waste Incineration
Exhaust Volume	64,400 ACFM
Exhaust Temperature	147°F saturated
Exhaust Pressure	3.0"W.C. (<1.0 per stage)
Contaminant	HCl, Cl_2, HBr Submicron Particulate
Removal Efficiency	Acid Gases > 99.9% Particulate > 98% (<0.003 gr/ DSCF)
Scrubbing Solution	Dilute NaOH solution
Materials of Construction	FRP & Polypropylene

VERANTIS Environmental Solutions Group

14955 Sprague Road, Suite 250 • Cleveland, OH 44136 USA
Ph: 440-243-0700 • TF: 800-924-0054 • Fax: 440-243-9854
E-mail: Case@Verantis.com

Verantis CO2/S0x/N0x removal

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Operational Experience of Commercial, Full Scale Ammonia-Based Wet FGD for Over a Decade

Amy P. Evans
Director of Technology
Marsulex Environmental Technologies Corporation

Claudia Miller
Technical Services Manager
Dakota Gasification Company

Steve Pouliot
Operations Manager
Dakota Gasification Company

Introduction

A novel and commercially viable process for flue gas desulfurization (FGD), using ammonia as a reagent and producing commercial grade ammonium sulfate (AS) crop fertilizer, was developed by General Electric Environmental Services, Inc. (GEESI) in the early 1990's and subsequently acquired by Marsulex Environmental Technologies (MET). The first field pilot of this technology was successfully executed at Dakota Gasification Company's (DGC) Synfuels Plant and led to a subsequent full-scale commercial installation of 350 MWe at that site. The DGC ammonia-based FGD system has been scrubbing flue gas from plant boilers while producing saleable fertilizer under the DakSul 45® label for well over 10 years now. Although this emergent technology was not immediately embraced by electric utilities in favor of conventional-type FGD systems, a second full-scale system (315 MWe) was placed into operation in late 2006 at an oil sand processing facility in Canada and a third system was sold in the People's Republic of China in 2008. Interest in this FGD approach is increasing today from both abroad (with a fourth system being negotiated for a coal-fired power plant in Eastern Europe) and by increasing inquiries regarding potential U.S. utility coal application. Reasons for the renewed interest in this technology include: the demonstrated commercial, full-scale success of the process; operational reliability and SO_2 scrubbing equal to or greater than conventional wet FGD; offsets to a portion of the yearly operating costs derived by the sale of the AS fertilizer by-product; and the CO_2

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The Unique Challenge of Controlling Biomass-Fired Boilers

Biofuel's Popularity

5. Biomass Conversion Technologies

Marsulex experience **Biomass control issues** **Biomass/coal combustion**

An example of the range of products which can be produced through emissions capture is provided below. The same array to be used in the proposed plant for acid gas (S0x + CO2) emissions capture has been in continuous operation at this facility, the Dakota Gasification plant, for over 10 years, with major modifications now in place for the C02 capture downstream from the Marsulex wet scrubber:

http://www.dakotagas.com/Products/Product_Profiles/index.html

Respectfully submitted,

Walter James O'Brien

Power plant cost analyst

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